

# Water System Analysis

FOR:

# Weaver's Pointe Subdivision



## Narrative:

The proposed residential project is located on a 43.10 acre vacant, mostly wooded lot. The proposed development includes construction of 87 single family residential properties. The site is located in Zebulon, NC. The proposed water distribution system will tie to the existing 12" water lines located in the southern and eastern existing road stubs, and be extended into the development. A water system analysis has been performed in order to verify that the system meets all applicable rules regarding minimum pressures and flows.

## **Procedure:**

KY Pipe software was used to model the proposed water system. A pressure supply was used to simulate the existing system conditions, as determined by a hydrant flow test (results are included in Appendix A). The software analyses each hydrant junction in the model by determining the flow that is available at each junction. The model is then run to verify that the required minimum pressure of 30 psi is maintained for non-fire flow conditions.

## Fire Flow Requirements:

Per a meeting with the Garner Fire Department, a minimum system pressure of 20 psi shall be maintained, while providing a 500 gpm fire flow at each new hydrant.

## Domestic Demand only Requirements:

The NCDEQ requirements state that a minimum pressure of 30 psi be maintained in the proposed system for domestic demands (non-fire flow). The model was run using domestic demands only to verify that the pressure at all nodes exceeds 30 psi. A domestic demand of 1.3 gpm per lot was included, to represent the peak hour demand. The domestic demand was determined from the State Rules 15ANCAC 18C .0802 (table provided in Appendix D)

The domestic demands for the 87 single family lots were applied at the appropriate junctions in the system.

## **Results:**

The analysis shows that all hydrant junctions exceed the required flow of 500 gpm at a pressure of 20 psi. The provided flow at 20 psi ranges from 1,202 psi to 1,519 psi. The fire flow results are provided in Appendix C. The results also show that a minimum pressure of 30 psi is maintained in the proposed system for domestic demands only (non-fire flow). The non-fire flow results are provided in Appendix D.

Appendix A Hydrant Flow Test



### **TEST LOCATION**

Address/Location Description 600 Yulee Drive, Zebulon Test hydrant Facility ID WHYD 186269 Flow hydrant Facility ID WHYD 186267

#### **APPLICATION INFORMATION**

Name\_Futrell Development, LLCAddress\_4020 Wake Forest Road, Suite 102F, Raleigh, NC 27609Contact Person\_Grey BerryPhone\_919.606.8956Email\_grey@futrellproperty.com

#### SYSTEM INFORMATION

Test Date_	Septemb	er	13,	2023	
Nearest Ele	vated Tank_	Gr	een	Pace	
Main Size_	12"				
Tank Hydra	ulic Grade	44	9.3'		
Pump Info	Wendell	lв	ypas	s Pl	

Time of Test 11:30 AM Test Hydrant Elevation 368' +/-Pressure Zone 462' Use 20ft below pressure zone (tank overflow) for design\* Theoretical Pressure 35.2 psi

#### RESULTS

Static Pressure36psiResidual Pressure29psiOutlet Diameter2inches

Number of Outlets Flowing2Flow Hydrant Discharge Pressure9,10Volume of Discharge494 + 521 = 1,015gpmWater usage during test $5,100^{+/-}$ Total Gal

Test Completed by: Drew King & Danny Wilder Testing Company: Associated Fire Protection Checked by: N/A Date 9/13/2023

Notes: Flowed (2) 2-1/2" Hose Monster(s) with 2" Pitotless Nozzle(s). C = 1.38



Please attach the following supporting documentation to this form; Labeled map of location of test identifying test hydrant and flow hydrant Calculation demonstrating how the discharge flow was determined Calculation demonstrating the available fire flow at a residual pressure of 20 psi Printout of any recorded data supporting the static and residual pressure at the test hydrant. Printout of any recorded data supporting the discharge pressure of the flow hydrant.

\*To maintain system water quality, storage tanks may be maintained as low as 20' below overflow.

updated February 2020

# 600 Yulee Drive



Lee Kimmel, Sarah Lanier, Andrew Hayes, City of Raleigh GIS

# **Hydrant Flow Test Report**

Test Date 9/13/2023

## **Location**

Purdy Family Property 600 Yulee Drive Zebulon, NC

## Tested by

Associated Fire Protection PO Box 28022 Raleigh, NC 27611 DKing@afp-nc.com 919-906-5236

Test Time 11:30 AM

## Read Hydrant

36 psi **static pressure** 29 psi **residual pressure** 368 ft **hydrant elevation** 



Created with the free hydrant flow test program from www.igneusinc.com

## Notes

	•	
2"		
<b>PITOTLESS NOZZ</b>		TM
PN2THD		
FLOW CHART	1	

AOPS	2" 40	elli n Atr	Nº /	TOPE	1 2" HO	sell Armo	HOW	2" HC	Let II Atmo
0	22/ 200	Open	/	41	22/ 100	Open	ter	2.11 MC	o open
PSI	GPM	GPM		PSI	GPM	GPM	GPM	PSI	PSI
0	521	529		41	1055	1071	500	9.5	9.1
11	547	555		42	1068	1084	562.5	11.7	11.3
12	571	579		43	1081	1096	750	20.7	20.1
3	594	603		44	1093	1109	1000	36.8	35.8
4	617	626		45	1106	1122	1125	46.6	45.3
15	638	648	an ar as	46	1118	1134	1500	82.8	80.5
6	659	669		47	1130	1146	The readings on this chart are	based on which	h device the Pitotless Nozzle
17	679	689	是有效的	48	1142	1158	is connected to.	verify that the	correct chart and column is
8	699	709		49	1154	1170	being used. • 2 ½" Hose Monster M	odel II or Flush	er with flow solitter (HM2H
9	718	729		50	1165	1182	HM2HF). Use this colur 2 %" Hose Monster or F	nn if the Pitotle	ss Nozzle is connected to the
20	737	748		51	1177	1194	be installed for accurac	y. If you do not	have the built-in pitot or flow
21	755	766		<b>52</b>	1188	1206	Open Atmosphere. U     connected directly to a	se this column v	when the Pitotless Nozzle is
22	773	784		53	1200	1217	atmosphere.	test neader of 1	ryurant nowing openny to
23	790	802		54	1211	1229	This chart is FM Approved for	flow rate accurate	acy. Please call us or instruct
24	807	819		55	1222	1240	Additional copies of flow char	ts are available	at:
25	824	836		56	1233	1251	www.hosemonstel.commerature.h	um	
26	840	853		57	1244	1262			TH
27	856	869		58	1255	1273			APPROVED
28	872	885		59	1266	1284			
29	887	900		60	1277	1295			
30	903	916		61	1287	1306			
31	918	931		62	1298	1317	A The	Pitolless Nozzi 2"	(Comp)
32	932	946		63	1308	1327	-	Via Patente Calla STA Vias Patente Anglanda, Mil.	-
33	947	960		64	1318	1338		IN DO-DUIDE	
34	961	975		65	1329	1348			
35	975	989		66	1339	1358			
36	989	1003	and the second s	67	1349	1369	-	* The	100
37	1002	1017		68	1359	1379		HO	SE
38	1016	1031		69	1369	1389		NST	ER
39	1029	1044		70	1379	1399		MDA	NY
10	1042	1057					Divisio	n of Hydro Flow Proc	Bucis, Inc. Lindated Jun. 2015

 $Q = \sqrt{P \times k}$ K = 164.8

 $\begin{array}{r} 3psi \approx 285 \\ 4 \approx 330 \\ 5 \approx 369 \end{array}$ 

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404

436

466

494

6

7

8

9

MANUFACTURED BY: Hydro Flow Products, Inc. 888.202.9987 TOLL FREE 847.434.0073 FAX Service@FlowTest.com EMAIL www.HoseMonster.com

U. S. Patent # 6,874,375

## **Calculating Flow-rates**

The flow charts we provide with the Pitotless Nozzle<sup>™</sup>, Hose Monster<sup>®</sup> and Nozzle Inserts are correct and should be referred to first. Our flow charts are calculated using K-Factors derived from testing performed at FM Approvals. It is common for third-party software to use the pitot formula to compute flow-rate. The 2½ " Hose Monster uses a pitot to measure velocity pressure. The Pitotless Nozzle and 4" and 4½ " Hose Monsters do not use a pitot, and the pitot formula has to be tricked into calculating correct flow-rates. Entering the coefficients into a program that uses orifice diameter, coefficient and velocity pressure should give relatively accurate flow-rates. Check results against our flow charts.

Here are the equations used for calculating flow-rates and predicting flow-rates. Use the orifice diameter, coefficient or K-factor found on the next page.

## **K-factor Formula**

Computes a flow-rate in GPM given a psi and a K-factor of the flow device.

 $\mathbf{Q} = \sqrt{\mathbf{P} \mathbf{x} \mathbf{K}}$ 

Q = flow-rate in GPM, P = velocity pressure in psi, K = K-factor of flow device

## **Pitot Formula**

Computes a flow-rate in GPM given a psi and coefficient of the flow device.

 $Q = 29.84 \text{ x} \sqrt{P} \text{ x} D^2 \text{ x} C$ 

Q = flow-rate in GPM, P = velocity pressure in psi, D = orifice diameter in inches

C = coefficient of flow device

### **Equation for Determining Rated Capacity**

#### Computes the flow-rate available at a specified residual pressure (a.k.a. Rated Capacity).

The example below enables you to find the predicted flow-rate at 20 psi residual pressure.

 $Q_{R} = Q_{F} \times (H_{R}^{0.54} / H_{F}^{0.54})$ 

- $Q_{R}$  = Flow-rate predicted at the desired residual pressure in GPM
- Q<sub>F</sub> = Total test flow-rate measured during test in GPM (GPM measured from Hose Monster or Pitotless Nozzle)
- H<sub>R</sub> = Pressure drop from static pressure to desired residual pressure (Static 20 psi [if 20 psi is the desired residual pressure])
- $H_{F}$  = Actual pressure drop measured during the test (Static Actual Residual)

(Source: NFPA 291, 2010)

## **Conversion Factors**

#### Here are some conversion factors for switching between US and metric units:

### Flow-rate:

Pressure:

US Gallons per Minute x 3.785 = Liters per Minute Liters per Minute x 0.264 = US Gallons per Minute

US Gallons per Minute x 0.1337 = Cubic Feet per Minute Cubic Feet per Minute x 7.481 = US Gallons per Minute

#### Volume:

US Gallons x 3.785 = Liters Liters x 0.264 = US Gallons

US Gallons x 0.8327 = Imperial Gallons Imperial Gallons x 1.201 = US Gallons

Cubic Feet x 7.48051945 = US Gallons US Gallons x 0.1337 = Cubic Feet psi x 0.0689 = Bars Bars x 14.5038 = psi

psi x 6894.757 = Pascals Pascals x 0.000145 = psi

Bars x 100,000 = Pascals Pascals x 0.00001 = Bars

#### Weight of Water:

US Gallons of Water x 8.3454 = Pounds Cubic Feet of Water x 62.42796 = Pounds

#### Length:

Meters x 3.2808 = Feet Feet x 0.3048 = Meters

# Coefficient and K-Factor Table for Various Flow Devices

last update: 2/14/2012

Pitotless Nozzle <sup>™</sup>					
Device	K-factor	Coefficient	Orifice Diameter	psi Range	Flow Range (GPM)
2 " Pitotless Nozzle + Little Hose Monster™	156.0	1.31	2 "	10–70	490–1300
2" Pitotless Nozzle + 21/2" Hose Monster Steel	164.8	1.38	2"	10-80	520-1380
2 " Pitotless Nozzle + Open Atmosphere	167.2	1.40	2 "	10–70	530-1400
1 <sup>3</sup> / <sub>4</sub> " Pitotless Nozzle + Little Hose Monster	104.7	1.15	1.75"	10–90	330-1000
1 <sup>3</sup> / <sub>4</sub> " Pitotless Nozzle + 2 <sup>1</sup> / <sub>2</sub> " Hose Monster Steel	106.6	1.17	1.75"	10–90	340-1010
1 <sup>3</sup> / <sub>4</sub> " Pitotless Nozzle + Open Atmosphere	109.7	1.20	1.75"	10–90	350-1040
1 <sup>1</sup> / <sub>8</sub> " Pitotless Nozzle + Little Hose Monster	37.2	0.98	1.125"	5–90	80–350
1 <sup>1</sup> / <sub>8</sub> " Pitotless Nozzle + 2 <sup>1</sup> / <sub>2</sub> " Hose Monster Steel	37.4	0.99	1.125"	5–90	80-350
1 <sup>1</sup> / <sub>8</sub> " Pitotless Nozzle + Open Atmosphere	37.0	0.98	1.125"	5–90	80–350
1 " Pitotless Nozzle + Little Hose Monster	27.2	0.91	1"	3–90	50-260
1 " Pitotless Nozzle + 21/2 " Hose Monster Steel	27.6	0.93	1"	3–90	50–260
1 "Pitotless Nozzle + Open Atmosphere	27.7	0.93	1"	3–90	50–260
In-Line Pitotless Nozzle™					
Device	K-factor	Coefficient	Orifice Diameter	psi Range	Flow Range (GPM)
2 " In-line Pitotless Nozzle	165.3	1.38	2 "	10–75	530-1430
1¾" In-line Pitotless Nozzle	109.9	1.20	1.75"	5–80	250–980
1 <sup>1</sup> / <sub>8</sub> " In-line Pitotless Nozzle	38.4	1.02	1.125"	5–70	90–320
BigBoy Hose Monster™					
Device	K-factor	Coefficient	Orifice Diameter	psi Range	Flow Range (GPM)
4 to 10 psi (BigBoy Hose Monster)	382.9	1.38	3.05 "	4–10	766–1211
11 to 36 psi (BigBoy Hose Monster)	376.0	1.35	3.05 "	11–36	1247-2256
37 to 53 psi (BigBoy Hose Monster)	372.0	1.34	3.05 "	37–53	2263–2708
Note: Due to the shape and size of the BigBoy Pitotless No.	zzle, the BigBoy	/ Hose Monster	uses three different k	-factors over its ope	rating range.
2½" Hose Monster®					
Device	K-factor	Coefficient	Orifice Diameter	psi Range	Flow Range (GPM)
2½" Hose Monster	168.67	0.906	2.5"	10–75	530-1460
1 <sup>3</sup> / <sub>4</sub> " Nozzle Insert	89.04	0.975	1.75"	10–75	280-770
1 <sup>1</sup> / <sub>8</sub> " Nozzle Insert	37.36	0.99	1.125"	10–75	120–320
4" and 4½" Hose Monster®					
Device	K-factor	Coefficient	Orifice Diameter	psi Range	Flow Range (GPM)
4½" Hose Monster	331.07	0.548	4.5"	10–75	1050–2870
4" Hose Monster	339.65	0.712	4"	10–75	1070–2940
Using Software					
Use the table below if you are using software that requires	the coefficient	input to be less	than '1.0'. Notice that	at the orifice diamete	er must be changed from
Device	CICHLE THIS IS HE		efficient	Ori	fice Diameter

Device	Coefficient	Office Diameter
2 "Pitotless Nozzle + Little Hose Monster	0.99	2.30"
2 "Pitotless Nozzle + 21/2" Hose Monster Steel	0.99	2.36"
2 " Pitotless Nozzle + Open Atmosphere	0.99	2.38"
1 <sup>3</sup> / <sub>4</sub> " Pitotless Nozzle + Little Hose Monster	0.99	1.88"
1¾" Pitotless Nozzle + 21/2" Hose Monster Steel	0.99	1.90 "
1 <sup>3</sup> / <sub>4</sub> " Pitotless Nozzle + Open Atmosphere	0.99	1.93 "

Note: If your software uses the Theoretical Discharge Formula, found in NFPA 291, 4.7.3, the coefficient of discharge can be used to produce flow rates that will match our flow charts.

A hand-held pitot directly at a h	ydrant outlet	Classifying and Marking of Hydrants				
Outlet Type	Coefficient	Rated Capacity at 20 psi	Class	Marking Color of Hydrant Tops and Nozzles		
Outlet smooth and rounded	0.9	≥1500 GPM	AA	Light Blue		
Outlet square and sharp	0.8	1000–1499 GPM	А	Green		
Outlet square and projecting into barrel	0.7	500–999 GPM	В	Orange		
If a stream straightener is used	0.95	≤499 GPM	С	Red		

The above are the NFPA hydrant classifications and color markings for various rated capacities. Source: NFPA 291, 5.1, 2010.

600 Yulee Drive, Zebulon flow test - Wednesday, September 13, 2023



Appendix B System Map



Appendix C Fire Flow Analysis Results

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* * * * * * * * * * * KYPIPE * * * * * * * * * * *
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 Pipe Network Modeling Software
*
*
 CopyRighted by KYPIPE LLC (www.kypipe.com)
 Version: 6.025 10/21/2013
*
 Serial #: 6-5043202
*
*
 Interface: Classic
*
 Licensed for Pipe2012
Date & Time: Tue Apr 16 16:44:44 2024
Master File : f:\projects\fdcwp9\water system analysis\weavers water system.KYP\weavers water system.P2K
          SUMMARY OF ORIGINAL DATA
          UNITS SPECIFIED
  FLOWRATE ..... = gallons/minute
  HEAD (HGL) ..... = feet
  PRESSURE ..... = psig
PIPELINE DATA
 STATUS CODE: XX -CLOSED PIPE CV -CHECK VALVE
```

LENGTH DIAMETER ROUGHNESS

354.1012.00120.0000382.008.00120.0000

(ft) (in) COEFF. LOSS COEFF.

MINOR

1,20

1.20

1.20

1.20

1.20

1.20

1.20

1.20

1.20

P-14

VP-1

NODE NAMES

J-7

#1 #2

J-4 J-3 J-2 J-7

PUMP/LOSS ELEMENT DATA

THERE IS A DEVICE AT NODE VP-1 DESCRIBED BY THE FOLLOWING DATA: (ID= 1) HEAD FLOWRATE EFFICIENCY

IIBAD	LTOMULTE	ELLICIPIAC	-1
(ft)	(gpm)	(%)	
83.08	0.00	75.00	(Default)
46.15	1586.00	75.00	(Default)
0.00	2400.00	75.00	(Default)

NODE DATA

PTPE

NAME

P-1

P-2

P-3

P-4

P-5

P-7

P-9

P-13

N N	IODE IAME	NODE TITLE	EXTERNAL DEMAND (gpm)	JUNCTION ELEVATION (ft)	EXTERNAL GRADE (ft)
	J-1		15.00	366.00	
	J-2		15.00	371.00	
	J-3		15.00	363.00	
	J-4		15.00	363.00	
0010		P			

Pipe2010 Analysis Report



			weave	ers water	r system	n					
J-5		15.00	364.00								
J-6		15.00	365.00								
J-7		15.00	365.00								
J-8		15.00	366.00								
VP-1			368.00		368.00						
		7 17 7									
001901 01	PIION D	AIA									
	and the second second	a select a second	anna sere annh	and and an an an an an	an an seasonaine						
OUTPUT SELECTION:	ALL RESULT	S ARE INCLU	DED IN TH	E TABULAI	TED OUTE	PUT					
MAXIMUM A	AND MINIMUM P	RESSURES	= 4	4							
MAXIMUM A	AND MINIMUM V	ELOCITIES	= !	5							
MAXIMUM A	AND MINIMUM H	EAD LOSS/10	00 = !	5							
CYCEEM CC	NETCUD	ATTON									
SISIEM CC	JNFIGOR	AIION									
			-	0							
NUMBER OF PIE	PES		P) =	9							
NUMBER OF ENI	D NODES	(	J) = 8	8							
NUMBER OF PRI	IMARY LOOPS .	(	L) = .	1							
NUMBER OF SUI	PPLY NODES	(	F) =	1							
NUMBER OF SUI	PPLY ZONES		Z) =	1							
							=				
Case: U											
RESULTS OBTAINED	AFTER 8 TI	RIALS: ACCU	RACY = 0.1	59885E-04	1						
C T M H T D M T (		DTDMT	ON (T.								
SIMULAIIC	JN DESC	RIPII		ADEL)							
PTPFLTNF	RESILT	S									
PIPELINE	RESULT	S									
PIPELINE	RESULT	S	CHECK WALL	VF							
P I P E L I N E STATUS CODE:	RESULT XX -CLOSED P	S IPE CV -	CHECK VAL	VE							
PIPELINE STATUS CODE:	R E S U L T XX -CLOSED P	S IPE CV -	CHECK VALV	VE	MINOD	TIME	IIT I MT /				
PIPELINE STATUS CODE: PIPE	R E S U L T XX -CLOSED P NODE NUI	S IPE CV - MBERS F	CHECK VALV LOWRATE	VE HEAD	MINOR	LINE	HL+ML/	HL/			
PIPELINE STATUS CODE: PIPE NAME	R E S U L T XX -CLOSED P NODE NUI #1	S IPE CV - MBERS F #2	CHECK VALV LOWRATE	VE HEAD LOSS	MINOR	LINE VELO.	HL+ML/ 1000	HL/ 1000			
PIPELINE STATUS CODE: PIPE NAME	R E S U L T XX -CLOSED P NODE NUI #1	S IPE CV - MBERS F #2	CHECK VAL LOWRATE gpm	VE HEAD LOSS ft	MINOR LOSS ft	LINE VELO. ft/s	HL+ML/ 1000 ft/f	HL/ 1000 ft/f			
PIPELINE STATUS CODE: PIPE NAME	R E S U L T XX -CLOSED P NODE NUI #1	S IPE CV - MBERS F #2	CHECK VAL LOWRATE gpm	VE HEAD LOSS ft	MINOR LOSS ft	LINE VELO. ft/s	HL+ML/ 1000 ft/f	HL/ 1000 ft/f	-		
P I P E L I N E STATUS CODE: P I P E N A M E  P-1	R E S U L T XX -CLOSED P NODE NUI #1 J-4	S IPE CV - MBERS F #2 J-3	CHECK VALV LOWRATE gpm 54.83	VE HEAD LOSS ft 0.00	MINOR LOSS ft 0.00	LINE VELO. ft/s	HL+ML/ 1000 ft/f 0.01	HL/ 1000 ft/f 0.01	_		
P I P E L I N E STATUS CODE: P I P E N A M E 	RESULT XX -CLOSED P NODE NUI #1 J-4 J-2	S IPE CV - MBERS F #2 J-3 J-7	CHECK VAL LOWRATE gpm 54.83 -20.17	VE HEAD LOSS ft 0.00 0.01	MINOR LOSS ft 0.00	LINE VELO. ft/s	HL+ML/ 1000 ft/f 0.01 0.02	HL/ 1000 ft/f 0.01 0.02	-		
P I P E L I N E STATUS CODE: P I P E N A M E 	R E S U L T XX -CLOSED P NODE NUI #1 J-4 J-2 J-4	S IPE CV - MBERS F #2 	CHECK VALV LOWRATE gpm 54.83 -20.17 50.17	VE HEAD LOSS ft 0.00 0.01	MINOR LOSS ft 0.00 0.00	LINE VELO. ft/s	HL+ML/ 1000 ft/f 0.01 0.02 0.01	HL/ 1000 ft/f 0.01 0.02 0.01	- 1		
P I P E L I N E STATUS CODE: P I P E N A M E  P-1 P-2 P-3 P-4	R E S U L T XX -CLOSED P NODE NUI #1 J-4 J-2 J-4 J-2 J-4	S IPE CV – MBERS F #2 J-3 J-7 J-7 J-7	CHECK VALV LOWRATE gpm 54.83 -20.17 50.17	VE HEAD LOSS ft 0.00 0.01 0.00	MINOR LOSS ft 0.00 0.00 0.00	LINE VELO. ft/s	HL+ML/ 1000 ft/f 0.01 0.02 0.01	HL/ 1000 ft/f 0.01 0.02 0.01	- 1		
P I P E L I N E STATUS CODE: P I P E N A M E  P-1 P-2 P-3 P-4 P-4	R E S U L T XX -CLOSED P NODE NUI #1 J-4 J-2 J-4 J-3	S IPE CV - MBERS F #2 J-3 J-7 J-7 J-7 J-7 J-5	CHECK VAL LOWRATE gpm 54.83 -20.17 50.17 39.83	VE HEAD LOSS ft 0.00 0.01 0.00 0.00 0.00	MINOR LOSS ft 0.00 0.00 0.00 0.00	LINE VELO. ft/s 0.16 0.13 0.14 0.11	HL+ML/ 1000 ft/f 0.01 0.02 0.01 0.01	HL/ 1000 ft/f 0.01 0.02 0.01 0.01	-		
P I P E L I N E STATUS CODE: P I P E N A M E  P-1 P-2 P-3 P-4 P-5	R E S U L T XX -CLOSED P NODE NUI #1 J-4 J-2 J-4 J-3 J-5	S IPE CV - MBERS F #2 J-3 J-7 J-7 J-7 J-5 J-6	CHECK VAL LOWRATE gpm 54.83 -20.17 50.17 39.83 24.83	VE HEAD LOSS ft 0.00 0.01 0.00 0.00 0.00 0.00	MINOR LOSS ft 0.00 0.00 0.00 0.00 0.00	LINE VELO. ft/s 0.16 0.13 0.14 0.11 0.07	HL+ML/ 1000 ft/f 0.01 0.02 0.01 0.01 0.01	HL/ 1000 ft/f 0.01 0.02 0.01 0.01 0.00	-		
P I P E L I N E STATUS CODE: P I P E N A M E 	R E S U L T XX -CLOSED P NODE NUI #1 J-4 J-2 J-4 J-3 J-5 VP-1	S IPE CV – MBERS F #2 J-3 J-7 J-7 J-7 J-5 J-5 J-6 J-4	CHECK VALV LOWRATE 54.83 -20.17 50.17 39.83 24.83 120.00	VE HEAD LOSS ft 0.00 0.01 0.00 0.00 0.00 0.02	MINOR LOSS ft 0.00 0.00 0.00 0.00 0.00 0.00	LINE VELO. ft/s 0.16 0.13 0.14 0.11 0.07 0.34	HL+ML/ 1000 ft/f 0.01 0.02 0.01 0.01 0.00 0.00	HL/ 1000 ft/f 0.01 0.02 0.01 0.01 0.00 0.00	-		
P I P E L I N E STATUS CODE: P I P E N A M E  P-1 P-2 P-3 P-4 P-5 P-7 P-9	R E S U L T XX -CLOSED P NODE NUI #1 J-4 J-2 J-4 J-2 J-4 J-3 J-5 VP-1 J-7	S IPE CV – MBERS F #2 J-3 J-7 J-7 J-7 J-5 J-6 J-6 J-4 J-8	CHECK VALV LOWRATE 54.83 -20.17 50.17 39.83 24.83 120.00 15.00	VE HEAD LOSS ft 0.00 0.01 0.00 0.00 0.00 0.02 0.00	MINOR LOSS ft 0.00 0.00 0.00 0.00 0.00 0.00 0.00	LINE VELO. ft/s 0.16 0.13 0.14 0.11 0.07 0.34 0.04	HL+ML/ 1000 ft/f 0.01 0.02 0.01 0.01 0.00 0.00 0.00 0.00	HL/ 1000 ft/f 0.01 0.02 0.01 0.01 0.01 0.00 0.06 0.00	- 1		
P I P E L I N E STATUS CODE: P I P E N A M E 	R E S U L T XX -CLOSED P NODE NUI #1 J-4 J-2 J-4 J-3 J-5 VP-1 J-7 J-6	S IPE CV – MBERS F #2 J-3 J-7 J-7 J-7 J-7 J-5 J-6 J-4 J-8 J-1	CHECK VAL LOWRATE gpm 54.83 -20.17 50.17 39.83 24.83 120.00 15.00 9.83	VE HEAD LOSS ft 0.00 0.01 0.00 0.00 0.00 0.02 0.00 0.00	MINOR LOSS ft 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0	LINE VELO. ft/s 0.16 0.13 0.14 0.11 0.07 0.34 0.04 0.06	HL+ML/ 1000 ft/f 0.01 0.02 0.01 0.01 0.00 0.00 0.00 0.00	HL/ 1000 ft/f 0.01 0.02 0.01 0.01 0.00 0.00 0.00 0.00	-		
P I P E L I N E STATUS CODE: P I P E N A M E  P-1 P-2 P-3 P-4 P-5 P-7 P-9 P-13 P-14	R E S U L T XX -CLOSED P NODE NUI #1 J-4 J-2 J-4 J-3 J-5 VP-1 J-7 J-6 J-1	S IPE CV – MBERS F #2 J-3 J-7 J-7 J-7 J-7 J-7 J-5 J-6 J-4 J-4 J-8 J-1 J-2	CHECK VAL LOWRATE gpm 54.83 -20.17 50.17 39.83 24.83 120.00 15.00 9.83 -5.17	VE HEAD LOSS ft 0.00 0.01 0.00 0.00 0.00 0.00 0.02 0.00 0.00	MINOR LOSS ft 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0	LINE VELO. ft/s 0.16 0.13 0.14 0.11 0.07 0.34 0.04 0.03	HL+ML/ 1000 ft/f 0.01 0.02 0.01 0.01 0.00 0.00 0.00 0.00	HL/ 1000 ft/f 0.01 0.02 0.01 0.01 0.00 0.00 0.00 0.00	-		
P I P E L I N E STATUS CODE: P I P E N A M E 	R E S U L T XX -CLOSED P NODE NUI #1 J-4 J-2 J-4 J-3 J-5 VP-1 J-7 J-6 J-1	S IPE CV – MBERS F #2 J-3 J-7 J-7 J-5 J-5 J-6 J-4 J-8 J-1 J-2	CHECK VALV LOWRATE 54.83 -20.17 50.17 39.83 24.83 120.00 15.00 9.83 -5.17	VE HEAD LOSS ft 0.00 0.01 0.00 0.00 0.00 0.02 0.00 0.00	MINOR LOSS ft 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0	LINE VELO. ft/s 0.16 0.13 0.14 0.11 0.07 0.34 0.04 0.06 0.03	HL+ML/ 1000 ft/f 0.01 0.01 0.00 0.00 0.00 0.00 0.00 0.0	HL/ 1000 ft/f 0.01 0.02 0.01 0.00 0.00 0.00 0.00 0.00	-		
P I P E L I N E STATUS CODE: P I P E N A M E  P-1 P-2 P-3 P-4 P-5 P-7 P-9 P-13 P-14	R E S U L T XX -CLOSED P NODE NUI #1 J-4 J-2 J-4 J-2 J-4 J-3 J-5 VP-1 J-7 J-6 J-1	S IPE CV – MBERS F #2 J-3 J-7 J-7 J-7 J-5 J-6 J-6 J-4 J-8 J-1 J-2	CHECK VALV LOWRATE 9pm 54.83 -20.17 50.17 39.83 24.83 120.00 15.00 9.83 -5.17	VE HEAD LOSS ft 0.00 0.01 0.00 0.00 0.00 0.02 0.00 0.00	MINOR LOSS ft 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0	LINE VELO. ft/s 0.16 0.13 0.14 0.11 0.7 0.34 0.04 0.06 0.03	HL+ML/ 1000 ft/f 0.01 0.02 0.01 0.00 0.00 0.00 0.00 0.00	HL/ 1000 ft/f 0.01 0.02 0.01 0.01 0.00 0.06 0.00 0.00 0.00 0.00	- 1		
P I P E L I N E STATUS CODE: P I P E N A M E 	R E S U L T XX -CLOSED P NODE NUI #1 J-4 J-2 J-4 J-2 J-4 J-3 J-5 VP-1 J-7 J-7 J-6 J-1	S IPE CV – MBERS F #2 J-3 J-7 J-7 J-7 J-5 J-6 J-4 J-4 J-8 J-1 J-2	CHECK VAL LOWRATE gpm 54.83 -20.17 50.17 39.83 24.83 120.00 15.00 9.83 -5.17	VE HEAD LOSS ft 0.00 0.01 0.00 0.00 0.00 0.02 0.00 0.00	MINOR LOSS ft 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0	LINE VELO. ft/s 0.16 0.13 0.14 0.11 0.07 0.34 0.04 0.06 0.03	HL+ML/ 1000 ft/f 0.01 0.01 0.01 0.01 0.00 0.00 0.00 0.0	HL/ 1000 ft/f 0.01 0.02 0.01 0.01 0.00 0.00 0.00 0.00	-		
P I P E L I N E STATUS CODE: P I P E N A M E  P-1 P-2 P-3 P-4 P-5 P-7 P-9 P-13 P-14	R E S U L T XX -CLOSED P NODE NUI #1 J-4 J-2 J-4 J-3 J-5 VP-1 J-7 J-6 J-1	S IPE CV – MBERS F #2 J-3 J-7 J-7 J-7 J-7 J-5 J-6 J-4 J-4 J-8 J-1 J-2	CHECK VALV LOWRATE gpm 54.83 -20.17 50.17 39.83 24.83 120.00 15.00 9.83 -5.17	VE HEAD LOSS ft 0.00 0.01 0.00 0.00 0.00 0.00 0.02 0.00 0.00	MINOR LOSS ft 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0	LINE VELO. ft/s 0.16 0.13 0.14 0.11 0.07 0.34 0.04 0.06 0.03	HL+ML/ 1000 ft/f 0.01 0.02 0.01 0.01 0.00 0.00 0.00 0.00	HL/ 1000 ft/f 0.01 0.02 0.01 0.00 0.00 0.00 0.00 0.00	-		
P I P E L I N E STATUS CODE: P I P E N A M E  P-1 P-2 P-3 P-4 P-5 P-7 P-9 P-13 P-14 P U M P/L O S S	R E S U L T XX -CLOSED P NODE NUI #1 J-4 J-2 J-4 J-3 J-5 VP-1 J-7 J-6 J-1 E L E M E N	S IPE CV – MBERS F #2 J-3 J-7 J-7 J-7 J-5 J-6 J-4 J-8 J-4 J-8 J-1 J-2 T RES	CHECK VALV LOWRATE 54.83 -20.17 50.17 39.83 24.83 120.00 15.00 9.83 -5.17 ULT S	VE HEAD LOSS ft 0.00 0.01 0.00 0.00 0.00 0.02 0.00 0.00	MINOR LOSS ft 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0	LINE VELO. ft/s 0.16 0.13 0.14 0.11 0.07 0.34 0.04 0.06 0.03	HL+ML/ 1000 ft/f 0.01 0.01 0.00 0.00 0.00 0.00 0.00 0.0	HL/ 1000 ft/f 0.01 0.02 0.01 0.01 0.00 0.00 0.00 0.00	_		
P I P E L I N E STATUS CODE: P I P E N A M E 	R E S U L T XX -CLOSED P NODE NUI #1 J-4 J-2 J-4 J-3 J-5 VP-1 J-7 J-6 J-1 E L E M E N	S IPE CV - MBERS F #2 J-3 J-7 J-7 J-7 J-6 J-6 J-4 J-8 J-1 J-2 T RES	CHECK VALV LOWRATE 54.83 -20.17 50.17 39.83 24.83 120.00 15.00 9.83 -5.17 ULTS	VE HEAD LOSS ft 0.00 0.01 0.00 0.00 0.00 0.02 0.00 0.00	MINOR LOSS ft 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0	LINE VELO. ft/s 0.16 0.13 0.14 0.11 0.07 0.34 0.04 0.06 0.03	HL+ML/ 1000 ft/f 0.01 0.02 0.01 0.00 0.00 0.00 0.00 0.00	HL/ 1000 ft/f 0.01 0.02 0.01 0.00 0.00 0.00 0.00 0.00	- 1.		
P I P E L I N E STATUS CODE: P I P E N A M E 	R E S U L T XX -CLOSED P NODE NUI #1 J-4 J-2 J-4 J-3 J-5 VP-1 J-7 J-6 J-1 E L E M E N	S IPE CV - MBERS F #2 J-3 J-7 J-7 J-7 J-5 J-6 J-4 J-8 J-1 J-2 T RES	CHECK VAL LOWRATE gpm 54.83 -20.17 50.17 39.83 24.83 120.00 15.00 9.83 -5.17 U L T S	VE HEAD LOSS ft 0.00 0.01 0.00 0.00 0.00 0.00 0.00 0.0	MINOR LOSS ft 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0	LINE VELO. ft/s 0.16 0.13 0.14 0.11 0.07 0.34 0.04 0.06 0.03	HL+ML/ 1000 ft/f 0.01 0.01 0.01 0.00 0.00 0.00 0.00 0.0	HL/ 1000 ft/f 0.01 0.02 0.01 0.01 0.00 0.00 0.00 0.00	-		
P I P E L I N E STATUS CODE: P I P E N A M E 	R E S U L T XX -CLOSED P NODE NUI #1 J-4 J-2 J-4 J-3 J-5 VP-1 J-7 J-6 J-1 E L E M E N	S IPE CV – MBERS F #2 J-3 J-7 J-7 J-7 J-7 J-5 J-6 J-4 J-8 J-1 J-2 T RES	CHECK VAL LOWRATE gpm 54.83 -20.17 50.17 39.83 24.83 120.00 15.00 9.83 -5.17 U L T S	VE HEAD LOSS ft 0.00 0.01 0.00 0.00 0.00 0.00 0.00 0.0	MINOR LOSS ft 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0	LINE VELO. ft/s 0.16 0.13 0.14 0.11 0.07 0.34 0.04 0.06 0.03	HL+ML/ 1000 ft/f 0.01 0.01 0.01 0.00 0.00 0.00 0.00 0.0	HL/ 1000 ft/f 0.01 0.02 0.01 0.00 0.00 0.00 0.00 0.00	-		
P I P E L I N E STATUS CODE: P I P E N A M E 	R E S U L T XX -CLOSED P NODE NUI #1 J-4 J-2 J-4 J-3 J-5 VP-1 J-7 J-6 J-1 E L E M E N	S IPE CV - MBERS F #2 J-3 J-7 J-7 J-5 J-6 J-4 J-8 J-1 J-2 T RES T RES	CHECK VALV LOWRATE gpm 54.83 -20.17 50.17 39.83 24.83 120.00 15.00 9.83 -5.17 U L T S	VE HEAD LOSS ft 0.00 0.01 0.00 0.00 0.00 0.00 0.00 0.0	MINOR LOSS ft 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0	LINE VELO. ft/s 0.16 0.13 0.14 0.11 0.07 0.34 0.04 0.06 0.03	HL+ML/ 1000 ft/f 0.01 0.02 0.01 0.00 0.00 0.00 0.00 0.00	HL/ 1000 ft/f 0.01 0.02 0.01 0.00 0.00 0.00 0.00 0.00	- #ptimpg	ИРСН	Case
P I P E L I N E STATUS CODE: P I P E N A M E 	R E S U L T XX -CLOSED P NODE NUI #1 J-4 J-2 J-4 J-3 J-5 VP-1 J-7 J-6 J-1 E L E M E N INLE <sup>2</sup>	S IPE CV MBERS F #2 J-3 J-7 J-7 J-7 J-6 J-4 J-8 J-1 J-2 T RES T OUTLET	CHECK VALV LOWRATE gpm 54.83 -20.17 50.17 39.83 24.83 120.00 15.00 9.83 -5.17 U L T S PUMP HEDD	VE HEAD LOSS ft 0.00 0.01 0.00 0.00 0.00 0.00 0.00 0.0	MINOR LOSS ft 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0	LINE VELO. ft/s 0.16 0.13 0.14 0.01 0.07 0.34 0.04 0.06 0.03	HL+ML/ 1000 ft/f 0.01 0.01 0.00 0.00 0.00 0.00 0.00	HL/ 1000 ft/f 0.01 0.02 0.01 0.00 0.00 0.00 0.00 0.00	+PUMPS	NPSH	Case
P I P E L I N E STATUS CODE: P I P E N A M E 	R E S U L T XX -CLOSED P NODE NUI #1 J-4 J-2 J-4 J-3 J-5 VP-1 J-7 J-6 J-1 E L E M E N INLE RATE HEF	S IPE CV - MBERS F #2 J-3 J-7 J-7 J-7 J-6 J-4 J-4 J-8 J-1 J-2 T RES T RES T OUTLET D HEAD ft	CHECK VAL LOWRATE gpm 54.83 -20.17 50.17 39.83 24.83 120.00 15.00 9.83 -5.17 U L T S PUMP HEAD E+	<pre>HEAD LOSS ft 0.00 0.01 0.00 0.00 0.02 0.00 0.00 0.00</pre>	MINOR LOSS ft 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0	LINE VELO. ft/s 0.16 0.13 0.14 0.11 0.07 0.34 0.04 0.03 0.03	HL+ML/ 1000 ft/f 0.01 0.01 0.01 0.00 0.00 0.00 0.00 0.0	HL/ 1000 ft/f 0.01 0.02 0.01 0.00 0.00 0.00 0.00 0.00	#PUMPS SERIES	NPSH Avail.	Case
P I P E L I N E STATUS CODE: P I P E N A M E P-1 P-2 P-3 P-4 P-5 P-7 P-9 P-13 P-14 P U M P/L O S S NAME FLOWH gpr	R E S U L T XX -CLOSED P NODE NUI #1 J-4 J-2 J-4 J-3 J-5 VP-1 J-7 J-6 J-1 E L E M E N INLE RATE HEAN n ft	S IPE CV - MBERS F #2 J-3 J-7 J-7 J-7 J-7 J-7 J-7 J-7 J-7	CHECK VALV LOWRATE gpm 54.83 -20.17 50.17 39.83 24.83 120.00 15.00 9.83 -5.17 U L T S PUMP HEAD ft	VE HEAD LOSS ft 0.00 0.01 0.00 0.00 0.00 0.00 0.00 0.0	MINOR LOSS ft 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0	LINE VELO. ft/s 0.16 0.13 0.14 0.11 0.07 0.34 0.04 0.06 0.03 INCREMTI COST \$	HL+ML/ 1000 ft/f 0.01 0.02 0.01 0.00 0.00 0.00 0.00 0.00	HL/ 1000 ft/f 0.01 0.02 0.01 0.00 0.00 0.00 0.00 0.00	+PUMPS SERIES	NPSH Avail. ft	Case
P I P E L I N E STATUS CODE: P I P E N A M E P-1 P-2 P-3 P-4 P-5 P-7 P-9 P-13 P-14 P U M P/L O S S NAME FLOWE gpr	R E S U L T XX -CLOSED P NODE NUI #1 J-4 J-2 J-4 J-3 J-5 VP-1 J-7 J-6 J-1 E L E M E N INLE <sup>7</sup> RATE HEA n ft	S IPE CV - MBERS F #2 J-3 J-7 J-7 J-5 J-6 J-4 J-8 J-1 J-2 T RES T RES T OUTLET D HEAD ft	CHECK VALV LOWRATE gpm 54.83 -20.17 50.17 39.83 24.83 120.00 15.00 9.83 -5.17 U L T S PUMP HEAD ft	VE HEAD LOSS ft 0.00 0.01 0.00 0.00 0.00 0.00 0.00 0.0	MINOR LOSS ft 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0	LINE VELO. ft/s 0.16 0.13 0.14 0.07 0.34 0.04 0.06 0.03 INCREMTI COST \$	HL+ML/ 1000 ft/f 0.01 0.02 0.01 0.00 0.00 0.00 0.00 0.00	HL/ 1000 ft/f 0.01 0.02 0.01 0.00 0.00 0.00 0.00 0.00	#PUMPS SERIES	NPSH Avail. ft	Case
P I P E L I N E STATUS CODE: P I P E N A M E 	R E S U L T XX -CLOSED P NODE NUI #1 J-4 J-2 J-4 J-3 J-5 VP-1 J-7 J-6 J-1 E L E M E N INLE <sup>2</sup> RATE HEAN n ft 0.00 0.00	S IPE CV - MBERS F #2 J-3 J-7 J-7 J-7 J-6 J-4 J-8 J-1 J-2 T R E S T OUTLET D HEAD ft 0 82.84	CHECK VALV LOWRATE gpm 54.83 -20.17 50.17 39.83 24.83 120.00 15.00 9.83 -5.17 U L T S PUMP HEAD ft 	VE HEAD LOSS ft 0.00 0.01 0.00 0.00 0.02 0.00 0.00 0.00	MINOR LOSS ft 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0	LINE VELO. ft/s 0.16 0.13 0.14 0.01 0.07 0.34 0.04 0.06 0.03 INCREMTI COST \$ 1.0	HL+ML/ 1000 ft/f 0.01 0.01 0.00 0.00 0.00 0.00 0.00 0.0	HL/ 1000 ft/f 0.01 0.02 0.01 0.00 0.00 0.00 0.00 0.00	#PUMPS SERIES **	NPSH Avail. ft 33.2	Case 0.0000
P I P E L I N E STATUS CODE: P I P E N A M E 	$\begin{array}{cccccccccccccccccccccccccccccccccccc$	S IPE CV - MBERS F #2 J-3 J-7 J-7 J-7 J-5 J-6 J-4 J-8 J-1 J-2 T R E S T OUTLET D HEAD ft 0 82.84	CHECK VAL LOWRATE gpm 54.83 -20.17 50.17 39.83 24.83 120.00 15.00 9.83 -5.17 U L T S PUMP HEAD ft 82.8	<pre>HEAD LOSS ft 0.00 0.01 0.00 0.00 0.00 0.00 0.00 0.0</pre>	MINOR LOSS ft 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0	LINE VELO. ft/s 0.16 0.13 0.14 0.11 0.07 0.34 0.04 0.03 0.03 INCREMTI COST \$ 1.0	HL+ML/ 1000 ft/f 0.01 0.01 0.01 0.00 0.00 0.00 0.00 0.0	HL/ 1000 ft/f 0.01 0.02 0.01 0.00 0.00 0.00 0.00 0.00	#PUMPS SERIES **	NPSH Avail. ft 33.2	Case 0.0000
P I P E L I N E STATUS CODE: P I P E N A M E 	$\begin{array}{c} {\rm R} \ {\rm E} \ {\rm S} \ {\rm U} \ {\rm L} \ {\rm T} \\ {\rm XX} \ -{\rm CLOSED} \ {\rm P} \\ {\rm NODE} \ {\rm NUI} \\ \#1 \\ \\ {\rm J}-4 \\ {\rm J}-2 \\ {\rm J}-4 \\ {\rm J}-3 \\ {\rm J}-5 \\ {\rm VP}-1 \\ {\rm J}-7 \\ {\rm J}-6 \\ {\rm J}-1 \\ \end{array}$	S IPE CV - MBERS F #2 J-3 J-7 J-7 J-7 J-7 J-7 J-7 J-7 J-7	CHECK VALV LOWRATE gpm 54.83 -20.17 50.17 39.83 24.83 120.00 15.00 9.83 -5.17 U L T S PUMP HEAD ft 82.8	VE HEAD LOSS ft 0.00 0.01 0.00 0.00 0.00 0.00 0.00 0.0	MINOR LOSS ft 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0	LINE VELO. ft/s 0.16 0.13 0.14 0.11 0.07 0.34 0.04 0.06 0.03 INCREMTI COST \$ 1.0	HL+ML/ 1000 ft/f 0.01 0.02 0.01 0.00 0.00 0.00 0.00 0.00	HL/ 1000 ft/f 0.01 0.02 0.01 0.00 0.00 0.00 0.00 0.00	#PUMPS SERIES **	NPSH Avail. ft 33.2	Case 0.0000
P I P E L I N E STATUS CODE: P I P E N A M E 	$\begin{array}{cccccccccccccccccccccccccccccccccccc$	S IPE CV - MBERS F #2 J-3 J-7 J-7 J-5 J-6 J-4 J-8 J-1 J-2 T R E S T OUTLET D HEAD ft 0 82.84	CHECK VALV LOWRATE gpm 54.83 -20.17 50.17 39.83 24.83 120.00 15.00 9.83 -5.17 U L T S PUMP HEAD ft 82.8	VE HEAD LOSS ft 0.00 0.01 0.00 0.00 0.00 0.00 0.00 0.0	MINOR LOSS ft 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0	LINE VELO. ft/s 0.16 0.13 0.14 0.07 0.34 0.04 0.06 0.03 INCREMTI COST \$ 1.0	HL+ML/ 1000 ft/f 0.01 0.01 0.00 0.00 0.00 0.00 0.00 0.0	HL/ 1000 ft/f 0.01 0.02 0.01 0.00 0.00 0.00 0.00 0.00	#PUMPS SERIES **	NPSH Avail. ft 33.2	Case 0.0000
P I P E L I N E STATUS CODE: P I P E N A M E 	R E S U L T XX -CLOSED P NODE NUI #1 J-4 J-2 J-4 J-3 J-5 VP-1 J-7 J-6 J-1 E L E M E N INLE <sup>r</sup> RATE HEAD n ft 0.00 0.00	S IPE CV - MBERS F #2 J-3 J-7 J-7 J-7 J-6 J-4 J-8 J-1 J-2 T R E S T OUTLET D HEAD ft 0 82.84	CHECK VALV LOWRATE gpm 54.83 -20.17 50.17 39.83 24.83 120.00 15.00 9.83 -5.17 U L T S PUMP HEAD ft 82.8	VE HEAD LOSS ft 0.00 0.01 0.00 0.00 0.02 0.00 0.00 0.00	MINOR LOSS ft 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0	LINE VELO. ft/s 0.16 0.13 0.14 0.07 0.34 0.04 0.06 0.03 INCREMTI COST \$ 1.0	HL+ML/ 1000 ft/f 0.01 0.01 0.00 0.00 0.00 0.00 0.00 0.0	HL/ 1000 ft/f 0.01 0.02 0.01 0.00 0.00 0.00 0.00 0.00	#PUMPS SERIES **	NPSH Avail. ft 33.2	Case 0.0000
P I P E L I N E STATUS CODE: P I P E N A M E 	$\begin{array}{c} {\rm R} \ {\rm E} \ {\rm S} \ {\rm U} \ {\rm L} \ {\rm T} \\ {\rm XX} \ -{\rm CLOSED} \ {\rm P} \\ {\rm NODE} \ {\rm NUI} \\ \#1 \\ \\ {\rm J-4} \\ {\rm J-2} \\ {\rm J-4} \\ {\rm J-3} \\ {\rm J-5} \\ {\rm VP-1} \\ {\rm J-7} \\ {\rm J-6} \\ {\rm J-1} \\ \\ {\rm E} \ {\rm L} \ {\rm E} \ {\rm M} \ {\rm E} \ {\rm N} \\ \\ {\rm INLE}^{\rm r} \\ {\rm RATE} \\ {\rm n} \\ {\rm ft} \\ {\rm 0.00} \\ 0 \ {\rm 0.00} \end{array}$	S IPE CV - MBERS F #2 J-3 J-7 J-7 J-5 J-6 J-4 J-8 J-1 J-2 T R E S T OUTLET D HEAD ft 0 82.84	CHECK VAL LOWRATE gpm 54.83 -20.17 50.17 39.83 24.83 120.00 15.00 9.83 -5.17 U L T S PUMP HEAD ft 82.8	VE HEAD LOSS ft 0.00 0.01 0.00 0.00 0.00 0.00 0.00 0.0	MINOR LOSS ft 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0	LINE VELO. ft/s 0.16 0.13 0.14 0.11 0.07 0.34 0.04 0.06 0.03 INCREMTI COST \$ 1.0	HL+ML/ 1000 ft/f 0.01 0.02 0.01 0.00 0.00 0.00 0.00 0.00	HL/ 1000 ft/f 0.01 0.02 0.01 0.00 0.00 0.00 0.00 0.00	#PUMPS SERIES **	NPSH Avail. ft 33.2	Case 0.0000
P I P E L I N E STATUS CODE: P I P E N A M E 	R E S U L T XX -CLOSED P NODE NUI #1 J-4 J-2 J-4 J-3 J-5 VP-1 J-7 J-6 J-1 E L E M E N INLE RATE HEAM n ft 0.00 0.00	S IPE CV - MBERS F #2 J-3 J-7 J-7 J-7 J-7 J-7 J-7 J-7 J-7	CHECK VALV LOWRATE gpm 54.83 -20.17 50.17 39.83 24.83 120.00 15.00 9.83 -5.17 U L T S PUMP HEAD ft 82.8	VE HEAD LOSS ft 0.00 0.01 0.00 0.00 0.00 0.00 0.00 0.0	MINOR LOSS ft 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0	LINE VELO. ft/s 0.16 0.13 0.14 0.11 0.07 0.34 0.04 0.06 0.03 INCREMTI COST \$ 1.0	HL+ML/ 1000 ft/f 0.01 0.02 0.01 0.00 0.00 0.00 0.00 0.00	HL/ 1000 ft/f 0.01 0.02 0.01 0.00 0.00 0.00 0.00 0.00	+PUMPS SERIES **	NPSH Avail. ft 33.2	Case 0.0000
P I P E L I N E STATUS CODE: P I P E N A M E P-1 P-2 P-3 P-4 P-5 P-7 P-9 P-13 P-14 P U M P/L O S S NAME FLOWE GPT VP-1 120 N O D E R E S U NODE	$\begin{array}{c} {\rm R} \ {\rm E} \ {\rm S} \ {\rm U} \ {\rm L} \ {\rm T} \\ {\rm XX} \ -{\rm CLOSED} \ {\rm P} \\ {\rm NODE} \ {\rm NUI} \\ \#1 \\ \\ {\rm J}-4 \\ {\rm J}-2 \\ {\rm J}-4 \\ {\rm J}-3 \\ {\rm J}-5 \\ {\rm VP}-1 \\ {\rm J}-7 \\ {\rm J}-6 \\ {\rm J}-1 \\ \end{array}$	S IPE CV - MBERS F #2 J-3 J-7 J-7 J-5 J-6 J-4 J-8 J-1 J-2 T R E S T OUTLET D HEAD ft 0 82.84 EXTERNAL	CHECK VALV LOWRATE gpm 54.83 -20.17 50.17 39.83 24.83 120.00 15.00 9.83 -5.17 U L T S PUMP HEAD ft 82.8	VE HEAD LOSS ft 0.00 0.01 0.00 0.00 0.00 0.00 0.00 0.0	MINOR LOSS ft 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0	LINE VELO. ft/s 0.16 0.13 0.14 0.07 0.34 0.04 0.06 0.03 INCREMTI COST \$ 1.0	HL+ML/ 1000 ft/f 0.01 0.01 0.00 0.00 0.00 0.00 0.00 0.0	HL/ 1000 ft/f 0.01 0.02 0.01 0.00 0.00 0.00 0.00 0.00	#PUMPS SERIES **	NPSH Avail. ft 33.2	Case 0.0000
P I P E L I N E STATUS CODE: P I P E N A M E P-1 P-2 P-3 P-4 P-5 P-7 P-9 P-13 P-14 P U M P/L O S S NAME FLOWE gpr VP-1 120 N O D E R E S U NODE NAME	R E S U L T XX -CLOSED P NODE NUI #1 J-4 J-2 J-4 J-3 J-5 VP-1 J-7 J-6 J-1 E L E M E N INLE <sup>7</sup> RATE HEAN n ft 0.00 0.00 J L T S NODE TITLE	S IPE CV - MBERS F #2 J-3 J-7 J-7 J-7 J-6 J-4 J-8 J-1 J-2 T R E S T OUTLET D HEAD ft 0 82.84 EXTERNAL DEMAND	CHECK VALY LOWRATE gpm 54.83 -20.17 50.17 39.83 24.83 120.00 15.00 9.83 -5.17 U L T S PUMP HEAD ft 82.8 HYDRAULIC GRADE	VE HEAD LOSS ft 0.00	MINOR LOSS ft 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0	LINE VELO. ft/s 0.16 0.13 0.14 0.07 0.34 0.04 0.03 0.03 INCREMTI COST \$ 1.0	HL+ML/ 1000 ft/f 0.01 0.02 0.01 0.00 0.00 0.00 0.00 0.00	HL/ 1000 ft/f 0.01 0.02 0.01 0.00 0.00 0.00 0.00 0.00	#PUMPS SERIES **	NPSH Avail. ft 33.2	Case 0.0000
P I P E L I N E STATUS CODE: P I P E N A M E 	R E S U L T XX -CLOSED P: NODE NUI #1 J-4 J-3 J-5 VP-1 J-7 J-6 J-1 E L E M E N INLE RATE HEAN n ft 0.00 0.00 J L T S NODE TITLE	S IPE CV - MBERS F #2 J-3 J-7 J-7 J-5 J-6 J-4 J-8 J-1 J-2 T R E S T OUTLET D HEAD ft 0 82.84 EXTERNAL DEMAND gpm	CHECK VALY LOWRATE gpm 54.83 -20.17 50.17 39.83 24.83 120.00 15.00 9.83 -5.17 U L T S PUMP HEAD ft 82.8 HYDRAULIO GRADE ft	VE HEAD LOSS ft 0.00	MINOR LOSS ft 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0	LINE VELO. ft/s 0.16 0.13 0.14 0.11 0.07 0.34 0.04 0.03 0.03 INCREMTI COST \$ 1.0	HL+ML/ 1000 ft/f 0.01 0.02 0.01 0.00 0.00 0.00 0.00 0.00	HL/ 1000 ft/f 0.01 0.02 0.01 0.00 0.00 0.00 0.00 0.00	#PUMPS SERIES **	NPSH Avail. ft 33.2	Case 0.0000
P I P E L I N E STATUS CODE: P I P E N A M E P-1 P-2 P-3 P-4 P-5 P-7 P-9 P-13 P-14 P U M P/L O S S NAME FLOWE gpr VP-1 120 N O D E R E S U NODE NAME	R E S U L T XX -CLOSED P NODE NUI #1 J-4 J-2 J-4 J-3 J-5 VP-1 J-7 J-6 J-1 E L E M E N INLE RATE HEAM n ft 0.00 0.00 J L T S NODE TITLE	S IPE CV - MBERS F #2 J-3 J-7 J-7 J-7 J-5 J-6 J-4 J-8 J-1 J-2 T R E S T OUTLET D HEAD ft 0 82.84 EXTERNAL DEMAND gpm	CHECK VALV LOWRATE gpm 54.83 -20.17 50.17 39.83 24.83 120.00 15.00 9.83 -5.17 U L T S PUMP HEAD ft 82.8 HYDRAULIC GRADE ft	VE HEAD LOSS ft 0.00 0.01 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 75.00 C NODE ELEVATI ft	MINOR LOSS ft 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0	LINE VELO. ft/s 0.16 0.13 0.14 0.11 0.07 0.34 0.04 0.06 0.03 INCREMTI COST \$ 1.0 SSURE EAD PF tt	HL+ML/ 1000 ft/f 0.01 0.02 0.01 0.00 0.00 0.00 0.00 0.00	HL/ 1000 ft/f 0.01 0.02 0.01 0.00 0.00 0.00 0.00 0.00	#PUMPS SERIES **	NPSH Avail. ft 33.2	Case 0.0000
P I P E L I N E STATUS CODE: P I P E N A M E P-1 P-2 P-3 P-4 P-5 P-7 P-9 P-13 P-14 P U M P/L O S S NAME FLOWE GPT VP-1 120 N O D E R E S U NODE NAME	R E S U L T XX -CLOSED P NODE NUI #1 J-4 J-2 J-4 J-3 J-5 VP-1 J-7 J-6 J-1 E L E M E N INLE RATE HEA n ft D.00 0.00 J L T S NODE TITLE	S IPE CV - MBERS F #2 J-3 J-7 J-7 J-5 J-6 J-4 J-8 J-1 J-2 T RES T RES T OUTLET D HEAD ft 0 82.84 EXTERNAL DEMAND gpm	CHECK VALV LOWRATE gpm 54.83 -20.17 50.17 39.83 24.83 120.00 15.00 9.83 -5.17 U L T S PUMP HEAD ft 82.8 HYDRAULIO GRADE ft	VE HEAD LOSS ft 0.00 0.01 0.00	MINOR LOSS ft 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0	LINE VELO. ft/s 0.16 0.13 0.14 0.07 0.34 0.04 0.06 0.03 INCREMTI COST \$ 1.0	HL+ML/ 1000 ft/f 0.01 0.02 0.01 0.00 0.00 0.00 0.00 0.00	HL/ 1000 ft/f 0.01 0.02 0.01 0.00 0.00 0.00 0.00 0.00	#PUMPS SERIES **	NPSH Avail. ft 33.2	Case 0.0000
P I P E L I N E STATUS CODE: P I P E N A M E P-1 P-2 P-3 P-4 P-5 P-7 P-9 P-13 P-14 P U M P/L O S S NAME FLOWE GPT VP-1 120 N O D E R E S U NODE NAME Pipe2010 Analysis F	R E S U L T XX -CLOSED P NODE NUI #1 J-4 J-2 J-4 J-3 J-5 VP-1 J-7 J-6 J-1 E L E M E N INLE RATE HEAN n ft 0.00 0.00 J L T S NODE TITLE	S IPE CV - MBERS F #2 J-3 J-7 J-7 J-5 J-6 J-4 J-8 J-1 J-2 T R E S T OUTLET D HEAD ft 0 82.84 EXTERNAL DEMAND gpm	CHECK VALY LOWRATE gpm 54.83 -20.17 50.17 39.83 24.83 120.00 15.00 9.83 -5.17 U L T S PUMP HEAD ft 82.8 HYDRAULIC GRADE ft	VE HEAD LOSS ft 0.00	MINOR LOSS ft 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0	LINE VELO. ft/s 0.16 0.13 0.14 0.07 0.34 0.04 0.03 0.03 INCREMTI COST \$ 1.0 SSURE EAD PF t	HL+ML/ 1000 ft/f 0.01 0.02 0.01 0.00 0.00 0.00 0.00 0.00	HL/ 1000 ft/f 0.01 0.02 0.01 0.00 0.00 0.00 0.00 0.00	#PUMPS SERIES **	NPSH Avail. ft 33.2	Case 0.0000
P I P E L I N E STATUS CODE: P I P E N A M E P-1 P-2 P-3 P-4 P-5 P-7 P-9 P-13 P-14 P U M P/L O S S NAME FLOWE gpr VP-1 120 N O D E R E S U NODE NAME Pipe2010 Analysis F	R E S U L T XX -CLOSED P NODE NUI #1 J-4 J-3 J-5 VP-1 J-7 J-6 J-1 E L E M E N INLE RATE HEAN n ft 0.00 0.00 J L T S NODE TITLE	S IPE CV - MBERS F #2 J-3 J-7 J-7 J-5 J-6 J-4 J-8 J-1 J-2 T R E S T OUTLET D HEAD ft 0 82.84 EXTERNAL DEMAND gpm	CHECK VALY LOWRATE gpm 54.83 -20.17 50.17 39.83 24.83 120.00 15.00 9.83 -5.17 U L T S PUMP HEAD ft 82.8 HYDRAULIO GRADE ft	VE HEAD LOSS ft 0.00	MINOR LOSS ft 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0	LINE VELO. ft/s 0.16 0.13 0.14 0.11 0.07 0.34 0.04 0.03 0.03 INCREMTI COST \$ 1.0 SSURE LAD PF tt	HL+ML/ 1000 ft/f 0.01 0.02 0.01 0.00 0.00 0.00 0.00 0.00	HL/ 1000 ft/f 0.01 0.02 0.01 0.00 0.00 0.00 0.00 0.00	#PUMPS SERIES **	NPSH Avail. ft 33.2	Case 0.0000

					weaver	s water syst	em		
	3 3 3 3 3 3 3 3 3 3 7 4 9 4 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9	U-1 U-2 U-3 U-4 U-5 U-6 U-7 U-8 P-1		15.00 15.00 15.00 15.00 15.00 15.00 15.00 15.00	450.80 450.81 450.81 450.82 450.81 450.81 450.81 450.81	366.00 371.00 363.00 364.00 365.00 365.00 366.00 368.00	84.80 79.81 87.81 87.82 86.81 85.81 85.81 85.81 84.81 82.84	36.75 34.58 38.05 38.05 37.62 37.18 37.18 36.75 35.90	
						_			_
MA	XI	MUM AN	D MINI	MUM	VALUES			Domestic	
								Domand	
	PR	ESSURE	S					Demanu	
		JUNCTION NUMBER	MAXIMUM PRESSURES psi		JUNCTION NUMBER	MINIMUM PRESSURES psi			
		J-4 J-3 J-5 J-7	38.05 38.05 37.62 37.18		J-2 VP-1 J-1 J-8	34.58 35.90 36.75 36.75			
E	VE	LOCITI	ES						
		PIPE NUMBER	MAXIMUM VELOCITY (ft/s)		PIPE NUMBER	MINIMUM VELOCITY (ft/s)			
		P-7 P-1 P-3 P-2 P-4	0.34 0.16 0.14 0.13 0.11		P-14 P-9 P-13 P-5 P-4	0.03 0.04 0.06 0.07 0.11			
	H T.	+ M T. / 1	0 0 0						
	пп	- M L / I	000						
		PIPE NUMBER	MAXIMUM HL+ML/1000 (ft/ft)		PIPE NUMBER	MINIMUM HL+ML/1000 (ft/ft)			
		P-7 P-2 P-1 P-3 P-4	0.06 0.02 0.01 0.01 0.01		P-14 P-9 P-5 P-13 P-4	0.00 0.00 0.00 0.00 0.01			
	ΗL	/ 1000							
		PIPE NUMBER	MAXIMUM HL/1000 (ft/ft)		PIPE NUMBER	MINIMUM HL/1000 (ft/ft)			
		P-7 P-2 P-1 P-3 P-4	0.06 0.02 0.01 0.01 0.01		P-9 P-14 P-5 P-13 P-4	0.00 0.00 0.00 0.00 0.01			
S U (+) (-)	M M INFI OUTF N VP- SYSI	ARY OF LOWS INTO THI FLOWS FROM THI NODE F NAME	I N F L O E SYSTEM FRO HE SYSTEM IN LOWRATE gpm 120.00 = 120.00	WSA MSUPPLY TOSUPPLY NODE TITLE	N D O U T NODES Y NODES	FLOWS			
Pipe20	10 A	malysis Repo	ort						
<3>									

NET SYSTEM OUTFLOW = 0.00 NET SYSTEM DEMAND = 120.00

\_\_\_\_\_

weavers water system

\_\_\_\_\_

FireFlow/Hydrant Report Fireflow/Hydrant Report:

Specified Minimum Pressure(psi): 20.0 Minimum Static Pressure(psi) : 20.0 Sp.Min Pres@FirePump Suctn(psi): 0.0 Flow-1: Flowrate to maintain the specified pressure at (hydrant) node Node-2: Node that has a lower pressure than specified value at Flow-1 Flow-2: Flowrate to maintain the specified pressure at Node-2 Flow-3: Flowrate to maintain the specified pressure at Fire Pump Suction (Flow-3 is based on combined value of hydrant and hose constants)

Hose Constant = 0.00

Hydrant Node	Hydrant Constant	Elevation	Demand gpm	Static Pressure	Flow-1 gpm	Flow-2 gpm	Node-2	Flow-3 gpm	Flow Capacity	NFPA Color
J-1	0.0	366.0	15.0	36.7	1272.9					6
J-2	0.0	371.0	15.0	34.6	1202.4					
J-3	0.0	363.0	15.0	38.1	1479.3	1341.2	J-2			
J-4	0.0	363.0	15.0	38.1	1519.8	1352.4	J-2			
J-5	0.0	364.0	15.0	37.6	1426.1	1331.7	J-2			
J-6	0.0	365.0	15.0	37.2	1385.0	1324.8	J-2			
J-7	0.0	365.0	15.0	37.2	1437.6	1320.7	J-2			
J-8	0.0	366.0	15.0	36.8	1341.8	1320.7	J-2			
					$\bigwedge$		_			
				Ava	ailable	Flow				
				at 2	20 psi					



Pipe2010 Analysis Report

Appendix D Analysis Results with Domestic Demands Only



PEAK DEMAND FOR RESIDENTIAL COMMUNITY WATER SYSTEMS (Number of Connections vs Gallons per Minute)

Number of Connections

```
* * * * * * * * * * * KYPIPE * * * * * * * * * * *
*
*
 Pipe Network Modeling Software
*
*
 CopyRighted by KYPIPE LLC (www.kypipe.com)
 Version: 6.025 10/21/2013
*
 Serial #: 6-5043202
*
*
 Interface: Classic
*
 Licensed for Pipe2012
Date & Time: Wed Apr 17 08:31:47 2024
Master File : f:\projects\fdcwp9\water system analysis\weavers water system.KYP\weavers water system.P2K
          SUMMARY OF ORIGINAL DATA
          UNITS SPECIFIED
  FLOWRATE ..... = gallons/minute
  HEAD (HGL) ..... = feet
  PRESSURE ..... = psig
PIPELINE DATA
 STATUS CODE: XX -CLOSED PIPE CV -CHECK VALVE
                         LENGTH DIAMETER ROUGHNESS
 PTPE
                NODE NAMES
                                                MINOR
              #1 #2
                           (ft) (in) COEFF. LOSS COEFF.
 NAME
                         354.1012.00120.0000382.008.00120.0000
            J-4 J-3
J-2 J-7
    P-1
                                                 1,20
                     J-7
             P-2
                                                  1.20
    P-3
                                                 1.20
    P-4
                                                 1.20
    P-5
                                                  1.20
             VP-1
    P-7
                                                 1.20
    P-9
                                                 1.20
                                                 1.20
    P-13
```

1.20

PUMP/LOSS ELEMENT DATA

THERE IS A DEVICE AT NODE VP-1 DESCRIBED BY THE FOLLOWING DATA: (ID= 1) HEAD FLOWRATE EFFICIENCY

IILAD	L TOMICHI P	DEFICIDING	- L
(ft)	(gpm)	(%)	
83.08	0.00	75.00	(Default)
46.15	1586.00	75.00	(Default)
0.00	2400.00	75.00	(Default)

NODE DATA

<1>

P-14

NODE NAME	NODE TITLE	EXTERNAL DEMAND (gpm)	JUNCTION ELEVATION (ft)	EXTERNAL GRADE (ft)
J-1 J-2 J-3 J-4		15.00 15.00 15.00 15.00	366.00 371.00 363.00 363.00	
ipe2010 Analysis	Report			





	weave	ers water syst	*m	
	15.00 450.04	266.00	04.00 26.75	
	15.00 450.80	300.00	04.00 30.75 70.01 24.50	
	15.00 450.81	3/1.00	79.81 34.58	
	15.00 450.81	. 363.00	87.81 38.05	
	15.00 450.82	363.00	87.82 38.05	
	15.00 450.81	364.00	86.81 37.62	
	15.00 450.81	365.00	85.81 37.18	
	15.00 450.81	365.00	85.81 37.18	
	15.00 450.81	366.00	84.81 36.75	
	450.84	368.00	82.84 35.90	
AND MINI	MUM VALUE	S		
X E D				
MAXIMUM	JUNCTION	MINIMUM		
PRESSURES	NUMBER	PRESSURES		
psi		psi		
38.05	J-2	34.58		
38.05	VP-1	35.90		
37.62	J-1	36.75		
37.18	J-8	36.75		
ΓΙ Ε S				
MAXIMUM	PIPE	MINIMUM		
VELOCITY	NUMBER	VELOCITY		
(ft/s)		(ft/s)		
0.34	P-14	0.03		
0.16	P-9	0.04		
0.14	P-13	0.06		
0.13	P-5	0.07		
0.11	P-4	0.11		
1 0 0 0				
MAXIMUM	PIPE	MINIMUM		
HL+ML/1000	NUMBER	HL+ML/1000		
(ft/ft)		(ft/ft)		
0.06	P-14	0.00		
0.02	P-9	0.00		
0.01	P-5	0.00		
0.01	P-13	0.00		
0.01	P-4	0.01		
0.01		0.01		
0 0				
0 0 Maximim	PTPR	MINIMUM		
0 0 MAXIMUM HI/1000	PIPE NIMBEP	MINIMUM HI./1000		
0 0 MAXIMUM HL/1000 (ft/ft)	PIPE NUMBER	MINIMUM HL/1000 (ft/ft)		
0 0 MAXIMUM HL/1000 (ft/ft)	PIPE NUMBER	MINIMUM HL/1000 (ft/ft)		
0 0 MAXIMUM HL/1000 (ft/ft) 0.06	PIPE NUMBER  P-9	MINIMUM HL/1000 (ft/ft)		
0 0 MAXIMUM HL/1000 (ft/ft) 0.06 0.02	PIPE NUMBER  P-9 P-14	MINIMUM HL/1000 (ft/ft) 0.00 0.00		
0 0 MAXIMUM HL/1000 (ft/ft) 0.06 0.02 0 01	PIPE NUMBER  P-9 P-14 P-5	MINIMUM HL/1000 (ft/ft) 0.00 0.00		
0 0 MAXIMUM HL/1000 (ft/ft) 0.06 0.02 0.01 0.01	PIPE NUMBER  P-9 P-14 P-5 P-13	MINIMUM HL/1000 (ft/ft) 0.00 0.00 0.00 0.00		
0 0 MAXIMUM HL/1000 (ft/ft) 0.06 0.02 0.01 0.01 0.01	PIPE NUMBER  P-9 P-14 P-5 P-13 P-4	MINIMUM HL/1000 (ft/ft) 0.00 0.00 0.00 0.00 0.00		
	A N D M I N I R E S N MAXIMUM PRESSURES psi 38.05 38.05 37.62 37.18 T I E S MAXIMUM VELOCITY (ft/s) 0.34 0.16 0.14 0.13 0.11 1 0 0 0 MAXIMUM HL+ML/1000 (ft/ft) 0.06 0.02 0.01 0.01	15.00       450.81         10.00       JUNCTION         MAXIMUM       PIPE         NUMBER       P-14         0.16       P-9         0.14       P-13         0.13       P-5         0.11       P-4         10.00       MAXIMUM         HL+ML/1000       NUMBER         (ft/ft)	IS.00         450.01         J1.00           15.00         450.81         363.00           15.00         450.81         364.00           15.00         450.81         365.00           15.00         450.81         365.00           15.00         450.81         366.00           15.00         450.81         366.00            450.84         368.00           AND         MINIMUM         VALUES           RES         NUMER         PRESSURES           p31          36.75           J22         34.58           38.05         VP-1           38.05         VP-1           37.62         J-1           37.62         J-1           37.62         J-1           37.62         J-1           36.75         (ft/s)            (ft/s)            (ft/s)            (ft/s)            0.06           0.16         P-9           0.11         P-4           1000         MAXIMUM           HL+ML/1000         (ft/ft)           (ft/	A N D M I N I M U M V A L U E S N MAXIMUM V A L U E S MAXIMUM PIPE MINIMUM NUMBER VELOCITY (ft/s) 0.33.05 0.11 P-4 0.01 P-13 0.00 0.01 P-13 0.00 0.01 P-13 0.00 0.01 P-13 0.00 0.01 P-13 0.00 0.01 P-13 0.00 0.00 P-14 0.00 0.01 P-13 0.00 0.00 P-14 0.00 0.00 P-14 0.00 P-14 0.00 P-13 0.00 P-13 0.00 P-13 0.00 P-13 0.00 P-13 0.00 P-13 0.00 P-13 0.00 P-13 0.00 P-13 0.00 P-13 0.00 P-14 0.00 P-13 0.00 P-13 0.00 P-13 0.00 P-13 0.00 P-13 0.00 P-13 0.00 P-13 0.00 P-13 0.00 P-13 0.00 P-13 0.00 P-13 0.00 P-13 0.00 P-13 0.00 P-13 0.00 P-13 0.00 P-13 0.00



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weavers water system NET SYSTEM OUTFLOW = 0.00 NET SYSTEM DEMAND = 120.00 \_\_\_\_ ------Total Power Cost TOTAL POWER COST(\$) FOR THIS SIMULATION = 0.12 \*\*\*\*\* HYDRAULIC ANALYSIS COMPLETED \*\*\*\*\* Pipe2010 Analysis Report **KYPIPE** PIPE2012